

# A Review on Reforming Reactions with Emphasis on Methane Reforming

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## ABSTRACT

Methane reforming reactions are important for hydrogen production synthesis from natural gas. Three important types of reforming reactions are steam, oxygen and carbon dioxide reforming. Each of these reactions has its own advantages and disadvantages. Methane is favorite source of hydrogen. Fuel cells can directly convert chemical energy into fuel. Steam reforming of methane (SRM) is well established process to produce  $H_2$  for FC. In current review, research and studies on various aspects of reforming reactions are summarized.

**Key words:** Catalyst, activity, oxidation, Pressure, temperature.

## INTRODUCTION

The natural sources of fuels are depleting day by day. Other sources such as wind energy, solar energy are being explored. [1-5] The waste heat recovery, regeneration and co-generation are other means minimize heat requirement. [6-10] Hydrogen production in efficient manner is very important aspect in investigations in energy sector. Natural gas and crude oil contains Alkanes, (saturated hydrocarbons). There is a big challenge to researchers in direct conversion of methane, the dominating component in natural gas, into key chemical products. Fuel cells are being explored for hydrogen production. [11-15] Reforming or partial oxidation of natural gas producing synthesis gas is commonly used method for hydrogen production. Many technologies such as reforming of natural gas, Water electrolysis, gasification of coal, photo electrolysis, high temperature decomposition of water, biomass are being explored for hydrogen production. Many investigations are reported on reforming reactions. These investigations are aimed at

studying comparative yield by using different catalysts, sources of hydrogen and temperature conditions. The current review summarizes research and studies on reforming reactions.

## A REVIEW ON REFORMING REACTIONS WITH EMPHASIS ON METHANE REFORMING

An investigation was carried out by Zhang et.al. in order to improve a small-size gasification unit. [16] According to this research the reaction temperature has important impacts on semicoke catalyzed methane gas mixture. The catalytic activity of reforming can be enhanced by the addition of water vapor. The study carried out by them indicated that the semicoke can reduce the activation energy of the reforming reaction. Dong et.al studied methane reforming reactions over Ni/MgO catalyst for hydrogen production. [17] They carried out steam reforming of methane (SRM), partial oxidation of methane (POM), and oxy-steam reforming of methane (OSRM). The catalyst showed high activity and good stability in all the

reforming reactions. Fakeeha et.al evaluated the selectivity and yield of hydrogen over  $\gamma$ - $\text{Al}_2\text{O}_3$  supported and Sr promoted Ni based catalysts from  $\text{CH}_4$ - $\text{CO}_2$  reforming. [18] They observed that that selectivity and yield of  $\text{H}_2$  increased with the increase of reaction temperature and the optimum reaction temperature was  $700^\circ\text{C}$ . Dry reforming of methane over Nano Ni Polyol catalysts was investigated by Naeem et.al. [19] They produced syngas from the process. The dry methane reforming is considered environmental friendly due to the fact that, it utilizes two major greenhouse gases ( $\text{CH}_4$  and  $\text{CO}_2$ ). They prepared the catalyst in ethylene glycol medium with polyvinylpyrrolidone as a nucleation-protective agent. They produced the catalyst with high activity, stability and minimum coking rate during DRM.

According to Roh et.al the reforming methods attracting the researchers are, steam was reforming, oxy- $\text{CO}_2$  reforming. [20] Carcadea et.al carried out an investigation on steam methane reforming. [21] In their simulation studies, they considered two domains (reforming and permeating areas). In their investigation, they determined the maximum value of temperature in the sweep area of the porous membrane reactor. According to the results obtained by them, in the sweep area, the temperature was up to  $450^\circ\text{K}$ . The temperature, on the reforming side of the membrane was  $617^\circ\text{K}$ . Their study gave better knowledge of the reactions involved in steam methane reforming process. Halabi presented an experimental and modeling study for an improved process of sorption enhanced catalytic reforming. [22] In his investigation, he used novel catalyst/sorbent materials for low temperature high purity  $\text{H}_2$  with in situ  $\text{CO}_2$  capture. His investigation indicated that direct production of high  $\text{H}_2$  purity and fuel conversion ( $>99\%$ ) is achieved with low level of carbon oxides impurities ( $<100$  ppm). According to him, the enormous reduction of the reactor size, material loading, catalyst/sorbent ratio, and energy requirements are driving forces

behind use of Rh/Ce\_Zr1- $\alpha$   $\text{O}_2$  catalyst and  $\text{K}_2\text{CO}_3$ -promoted hydrotalcite process. Roh and Jun carried out an investigation on hydrogen production for fuel cells by low temperature methane steam reforming process. [23] According to their thermodynamic equilibrium analysis, it is possible to operate methane steam reforming at low temperatures. They proposed a scheme for the low temperature methane steam reforming. The scheme was aimed to produce  $\text{H}_2$  for fuel cells by burning both unconverted  $\text{CH}_4$  and  $\text{H}_2$  to supply the heat for steam methane reforming. From their investigation, it was concluded that that low temperature methane steam reforming is possible with stable activity.

Abdel-Aaland Abdelkreem explained challenges and progress in methane conversion. [24] According to them, there is an immense and powerful potential in efficient and economic conversion of methane to more valuable products. They discussed three routes. These routes of syngas ( $\text{CO}/\text{H}_2$ ) production provide two sub routes, methane to gasoline (Mobile) and hydrocarbons (Fisher-Tropsch) conversion. Other two options are catalytic methane decomposition, CMD and direct methane conversion, DMC. Munera et.al investigated the catalytic production of hydrogen through the carbon dioxide reforming of methane. [25] They carried out reaction in plug flow reactor and in a dense Pd/Ag membrane reactor. They studied the activity and stability of Pt/ $\text{La}_2\text{O}_3$  and compared it to the Rh/ $\text{La}_2\text{O}_3$  solids. They observed that the Rh (0.2%)/ $\text{La}_2\text{O}_3$  was much more stable than the Pt/ $\text{La}_2\text{O}_3$  formulations. Neiva and Gama discussed the importance of natural gas reforming. [26] According to them, the catalyst is an indispensable element in the reforming of the methane process. Catalyst carries out functions aimed to activate, accelerate, optimize, direct interactions or block interactions. Paul used LaCr1-,Ni,0<sub>3</sub> Perovskite catalysts for methane steam reforming. [27] He observed that catalysts work well from 700 to 900 K for methane

conversion. Also he observed that catalyst was more active at higher nickel content than at the lower nickel content. Ross carried out studies on the catalytic conversion of natural gas to useful products. [28] He discussed important subjects such as steam reforming, oxidative coupling and CO, reforming of methane. Emphasis of his studies was on the development of novel catalysts for these processes. According to him, steam reforming was a major use of natural gas for the production of hydrogen in the petrochemical industry and for methanol synthesis. Thermodynamic analysis of methane dry reforming was carried out by Ying. [29] He carried out an investigation on the thermodynamic aspect of methane dry reforming at reforming temperature from 500 to 1000K at atmospheric pressure. Also he studied reaction at different methane to carbon dioxide ratios. He used Gibbs free energy minimization method. The results of his experiments showed that the product distribution was affected by the temperature.

## CONCLUSION

Methane is favorite source of hydrogen. Fuel cells can directly convert chemical energy into fuel. Steam reforming of methane (SRM) is well established process to produce H<sub>2</sub> for FC. Reforming or partial oxidation of natural gas producing synthesis gas is commonly used method for hydrogen production. Many technologies such as reforming of natural gas, water electrolysis, gasification of coal, photo electrolysis, High temperature decomposition of water, biomass are being explored for hydrogen production. Many investigations are reported on reforming reactions. Research and studies on reforming reactions have been summarized in review.

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